



# Exercise 02: MER and problem table method Guidelines

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École Polytechnique Fédérale de Lausanne ME451 – Advanced Energetics 2018/2019 Prof. François Maréchal

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#### **Outline**

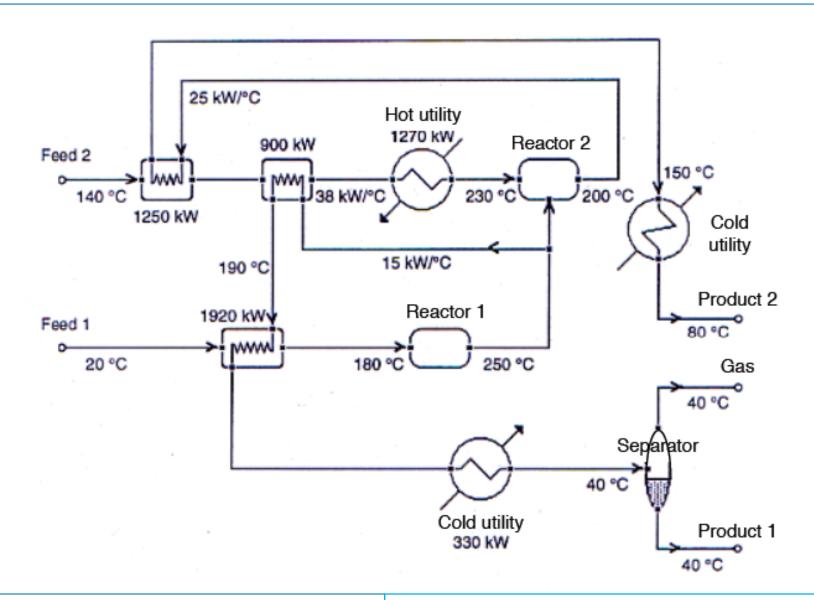
#### **FINAL GOAL:**

- 1. Estimate the energy bill of a process
- 2. Calculate the MER of a process by using the process table method
  - Draw the composite curves
  - Compute the heat cascade
  - Draw the grand composite curve
- 3. Estimate the possible energy saving under MER
- 4. Estimate the new energy bill under the MER
- 5. Identify the penalizing heat exchangers

#### System under study

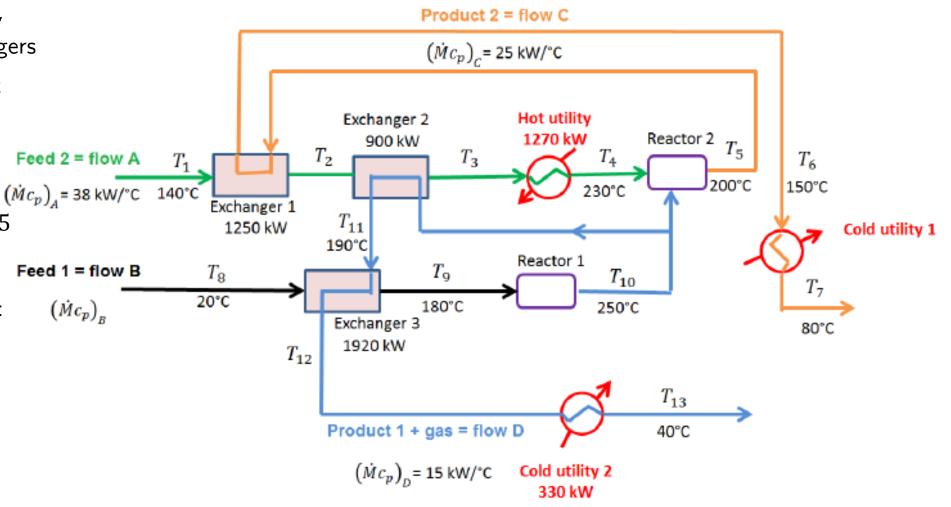
#### Industrial process composed by:

- 2 input feeds
- 2 output products + gas
- Heat exchanges
- Mixing/splitting
- Chemical reaction



#### QUESTION 1: actual energy bill

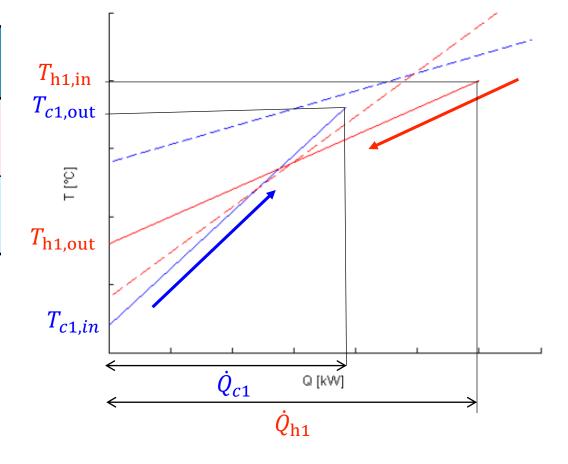
- Determine the missing temperatures  $T_2$ ,  $T_3$ ,  $T_{12}$  by heat balance at the exchangers
- Determine the missing heat capacity  $(\dot{M}c_p)_B$  by heat balance at Exchanger 3.
- Estimate the energy bill:
- 1. Hot utility: Boiler  $\eta = 0.85$   $OC_{boiler} \left[ \frac{CHF}{v} \right] ?$
- 2. Cold utility: cooling water:  $T_{cw,in} = 25 \, ^{\circ}\text{C}$   $T_{cw,out} = 35 \, ^{\circ}\text{C}$   $c_{p,cw} = 4.18 \, kJ/kg/K$   $\rho_{cw} = 996 \, kg/m^3$   $OC_{cw,} \left[\frac{CHF}{v}\right]$ ?



#### QUESTION 2: minimum energy requirements

1. Identify hot and cold streams: remember that an hot stream has to be cooled down while a cold stream has to be heated up.

Stream		T <sub>in</sub> [°C]	T <sub>out</sub> [°C]	$(\dot{M}c_p)$ [ $kW$ /°C]	<u>Q</u> [kW]
НОТ					
COLD					

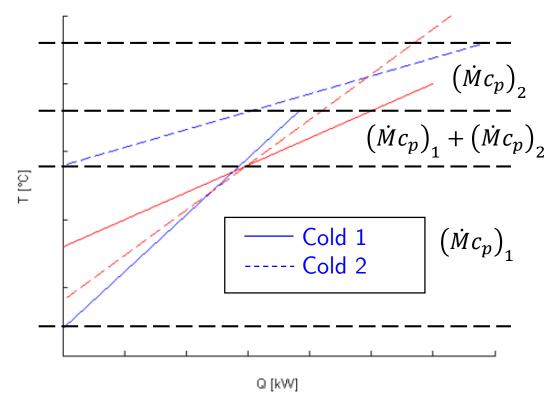


#### QUESTION 2: minimum energy requirements

1. Identify hot and cold streams: remember that an hot stream has to be cooled down while a cold stream has to be heated up.

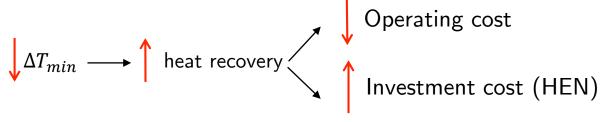
Stream		<i>T<sub>in</sub></i> [°C]	T <sub>out</sub> [°C]	$ig(\dot{M}c_pig) \ ig[kW/^\circ\! ext{C}ig]$	<u>Q</u> [kW]
НОТ					
COLD					

2. Define temperature intervals and sum up hot and cold streams respectively to obtain the **COMPOSITE CURVES** 

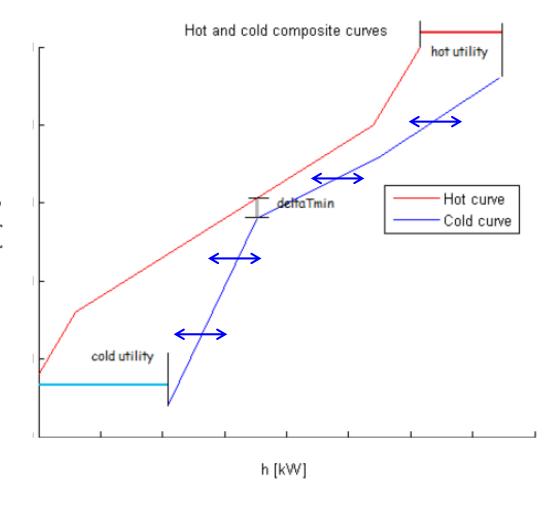


#### QUESTION 2: minimum energy requirement

- Hot and cold composite curves can be shifted horizontally
- Once the  $\Delta T_{min}$  is chosen hot and cold utility requirements are defined:



- $\Delta T_{min}$  is the result of an optimization: in this exercise test 5 values: 1, 3, 5, 10, 15 °C
- The minimum energy requirement can be estimated graphically
- Determine the MER more precisely with the problem table method



#### QUESTION 2: minimum energy requirement (problem table method)

1. Shift the hot and cold composite curves vertically of  $\Delta T_{min}/2$  so that they touch at the pinch point

Stream	$T_{in}$ [°C]	$T_{out}$ [°C]	$T_{in}^*$ [°C]	$T_{out}^*$ [°C]	$(\dot{M}c_p)$ [kW/°C]	<u> </u>
HOT 1			$T_{\mathrm{h}1,in} - \Delta T_{min}/2$	$T_{\rm h2,out} - \Delta T_{min}/2$		
HOT 2			$T_{\mathrm{h2},in} - \Delta T_{min}/2$	$T_{\rm h2,out} - \Delta T_{min}/2$		
COLD 1			$T_{c1,in} + \Delta T_{min}/2$	$T_{c1,out} + \Delta T_{min}/2$		
COLD 2			$T_{c2,in} + \Delta T_{min}/2$	$T_{\rm c2,out} + \Delta T_{min}/2$		

2. Build a table in terms of corrected temperatures intervals and check which streams are crossing each interval

#### QUESTION 2: minimum energy requirement (problem table method)

<b>T</b> * [°C]	$egin{array}{c} \Delta T_{r,r+1} \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \$	$\begin{bmatrix} \left( \dot{M} c_p \right)_{h1} \\ \left[ \frac{\mathbf{k} \mathbf{W}}{^{\circ} C} \right] \end{bmatrix}$	$ \frac{\left(\dot{M}c_{p}\right)_{h2}}{\left[\frac{\boldsymbol{k}\boldsymbol{W}}{^{\circ}C}\right]} $	$ \begin{pmatrix} \dot{M}c_p \\ c_1 \\ \hline \frac{\mathbf{k}\mathbf{W}}{^{\circ}\mathbf{C}} \end{bmatrix} $	$\begin{bmatrix} \left( \dot{M} c_p \right)_{c2} \\ \left[ \frac{\mathbf{k} \mathbf{W}}{^{\circ} \mathbf{C}} \right] \end{bmatrix}$	$ \left  \left( \dot{M} c_p \right)_{r,r+1} = \sum \dot{M} c_p \right  $ $ \left[ \frac{kW}{^{\circ}C} \right] $	$\Delta \dot{Q}_{r,r+1} \ [kW]$	$\dot{R}_{r}^{0}$ $[kW]$	Ř <sub>r</sub> [kW]
$T_1^*$								$\dot{R}_1^0 = 0$	
	$T_1^* - T_2^*$		$\left(\dot{M}c_{p}\right)_{h2}$		$\left(\dot{M}c_{p}\right)_{c2}$	$\left( \left( \dot{M}c_{p}\right) _{h2}-\left( \dot{M}c_{p}\right) _{c2}\right)$	$\left(\dot{M}c_{p}\right)_{1,2}\cdot\Delta T_{1,2}$		
$T_2^*$								$\dot{R}_2^0 = \dot{R}_1^0 + \Delta \dot{Q}_{1,2}$	

- 3. For each interval compute:
- The overall heat capacity  $(\dot{M}c_p)_{r,r+1} = \sum (\dot{M}c_p)_h \sum (\dot{M}c_p)_c$
- The heat load in each interval  $\Delta \dot{Q}_{r,r+1} = \left(\dot{M}c_p\right)_{r,r+1} \cdot \Delta T_{r,r+1}$
- The heat cascaded to the lower temperature interval  $\dot{R}^0_{r+1} = \dot{R}^0_r + \Delta \dot{Q}_{r,r+1}$
- Start with assumption  $\dot{R}_1^0 = 0$

## QUESTION 2: minimum energy requirement (problem table method)

<b>T</b> * [°C]	$\Delta T_{r,r+1}$ [°C]	$ \begin{pmatrix} \dot{M}c_p \\ \frac{\mathbf{k}\mathbf{W}}{^{\circ}\mathbf{C}} \end{pmatrix}^{h1} $	$ \begin{pmatrix} \dot{M}c_p \\ \frac{\mathbf{k}\mathbf{W}}{^{\circ}\mathbf{C}} \end{pmatrix}^{h2} $	$ \begin{pmatrix} \dot{M}c_p \\ c_1 \end{pmatrix}_{c1} \\ \left[ \frac{\mathbf{k}W}{^{\circ}C} \right] $	$ \left[ \frac{\left( \dot{M} c_p \right)_{c2}}{\left[ \frac{\mathbf{k} \mathbf{W}}{^{\circ} \mathbf{C}} \right]} \right] $	$ \left( \dot{M} c_p \right)_{r,r+1} = \sum \dot{M} c_p $ $ \left[ \frac{kW}{^{\circ}C} \right] $	$\Delta \dot{Q}_{r,r+1} \ [kW]$	$egin{aligned} \dot{R}_{r}^{0} \ [m{kW}] \end{aligned}$	$egin{aligned} \dot{R}_r \ [kW] \end{aligned}$
$T_1^*$								$\dot{R}_1^0 = 0$	
	$T_1^* - T_2^*$		$\left(\dot{M}c_{p}\right)_{h2}$		$\left(\dot{M}c_{p}\right)_{c2}$	$\left(\dot{M}c_p\right)_{h2}-\left(\dot{M}c_p\right)_{c2}$	$\left(\dot{M}c_{p}\right)_{1,2}\cdot\Delta T_{1,2}$		
$T_2^*$								$\dot{R}_2^0 = \dot{R}_1^0 + \Delta \dot{Q}_{1,2}$	
	$T_2^* - T_3^*$	$\left(\dot{M}c_{p}\right)_{h1}$				$\left(\dot{M}c_{p}\right)_{h1}$	$\left(\dot{M}c_{p}\right)_{2,3}\cdot\Delta T_{2,3}$		
$T_3^*$								$\dot{R}_3^0 = \dot{R}_2^0 + \Delta \dot{Q}_{2,3}$	
$T_r^*$				_			_		
	$\Delta T_{r,r+1}$						$\left(\dot{M}c_{p}\right)_{r,r+1}\cdot\Delta T_{r,r+1}$		
$T_{r+1}^*$								$\dot{R}_{r+1}^0 = \dot{R}_r^0 + \Delta \dot{Q}_{r,r+1}$	

#### QUESTION 2: minimum energy requirement (problem table method)

$\dot{R}_{r}^{0} \ [kW]$	$egin{aligned} \dot{R}_r \ [kW] \end{aligned}$
$\dot{R}_1^0 = 0$	$\dot{R}_1 = \dot{R}_1^0 + \left  \dot{R}_{j+1}^0 \right $
$\dot{R}_{2}^{0} = \dot{R}_{1}^{0} + \Delta \dot{Q}_{1,2}$	$\dot{R}_2 = \dot{R}_2^0 + \left  \dot{R}_{j+1}^0 \right $
$\dot{R}_3^0 = \dot{R}_2^0 + \Delta \dot{Q}_{2,3}$	
$\dot{R}_{j+1}^0 = \dot{R}_j^0 + \Delta \dot{Q}_{j,j+1} = \min \dot{R}_r^0$	$ \dot{R}_{j+1} = \dot{R}_{j+1}^0 +  \dot{R}_{j+1}^0  = 0$
$\dot{R}_{r+1}^0 = \dot{R}_r^0 + \Delta \dot{Q}_{r,r+1}$	

- Take the most negative value in the heat cascade
- Sum up this value to the heat cascaded at each interval (in absolute value)
- All  $\dot{R}_k$  will be positive
- The temperature at which  $\dot{R}_r = 0$  is the pinch point
- $\dot{R}_1$  defines the hot utility requirement
- $\dot{R}_{last}$  defines the cold utility requirement
- The plot  $\dot{R}_r$  vs  $T^*$  is the **GRAND COMPOSITE** CURVE

 $\mathsf{MER} = \dot{R}_1 + \dot{R}_{last}$ 

#### QUESTION 3: possible energy savings

- For each  $\Delta T_{min}$  the corresponding MER can be calculated
- Energy saving can be computed as the difference between the current energy requirement (from QUESTION 1) and the MER
- The energy recovered in each scenario can be computed as the difference between the total heat needed by the cold streams and the heat provided by the hot utility or the total heat that has to be removed from the hot streams and the one removed by the cold utility

$\Delta T_{min}$ [°C]	$\dot{Q}_{hot}[kW]$	$\dot{Q}_{cold}$ [kW]	$\dot{Q}_{recovered} [kW]$
Actual			
1			
3			
5			
10			
15			

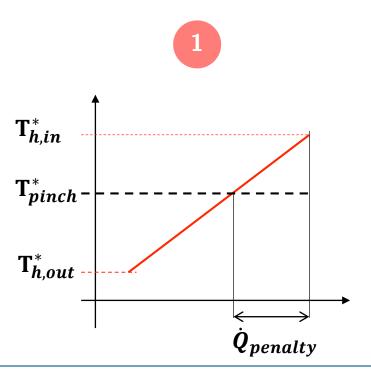
#### QUESTION 4: new energy bill

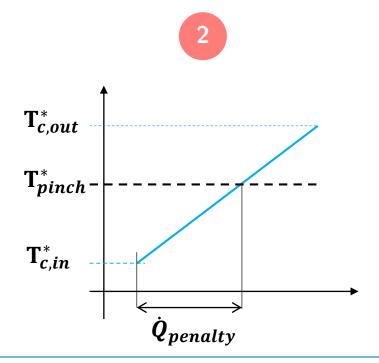
• Making the same assumption as for QUESTION 1, calculate the new energy bill for each  $\Delta T_{min}$ 

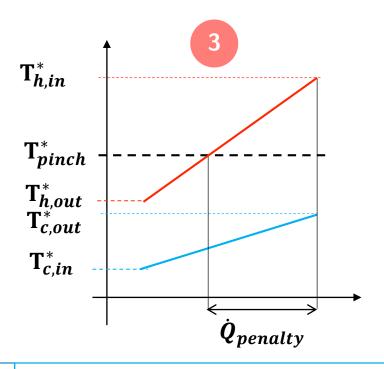
$\Delta T_{min}$ [°C]	$OC_{hot}[CHF/y]$	$OC_{cold}[CHF/y]$	OC [CHF/y]
Actual			
1			
3			
5			
10			
15			

#### QUESTION 5: penalizing heat exchangers

- The pinch point devides the system into two subsystems
- Once the pinch point is identified 3 rules must be checked:
- 1. NO COLD UTILITY ABOVE THE PINCH POINT → they will just increase the hot utility requirement
- 2. NO HOT UTILITY BELOW THE PINCH POINT → they will just increase the cold utility requirement
- 3. NO HEAT EXCHANGERS ACROSS THE PINCH POINT → they will increase the excessive heat below and reduce the available heat above







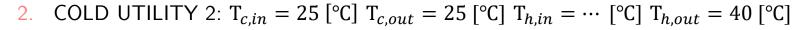
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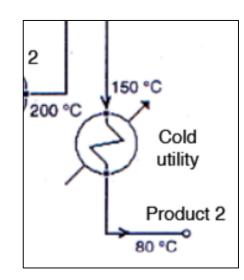
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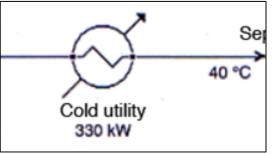
For all cold utilities check that the process hot stream inlet T is NOT above the pinch:

1. COLD UTILITY 1:  $T_{c,in} = 25$  [°C]  $T_{c,out} = 25$  [°C]  $T_{h,in} = 150$  [°C]  $T_{h,out} = 80$  [°C]

$\Delta T_{min}$ [°C]	$T^*_{pinch}$ [°C]	$T^*_{h,in}$ [°C]	$T^*_{h,out}$ [°C]	Penalizing? yes/no
1				
3				
5				
10				
15				







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For all hot utilities check that the process cold stream outlet T is not below the pinch

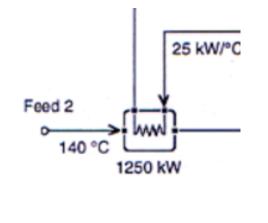
3. NO HEAT EXCHANGERS ACROSS THE PINCH POINT → they will increase the excessive heat below and reduce the available heat above

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- 3. NO HEAT EXCHANGERS ACROSS THE PINCH POINT  $\rightarrow$  they will increase the excessive heat below and reduce the available heat above

For each HEX check that none of the stream is crossing the pinch

$\Delta T_{min}$ [°C]	$T^*_{pinch}$ [°C]	$T_{c,in}^*$ [°C]	$T_{c,out}^*$ [°C]	$T_{h,in}^*$ [°C]	$T_{h,out}^*$ [°C]	Penalizing? yes/no
1						
3						
5						
10						
15						



#### Conclusions

- The problem table method is a systematic and powerful procedure to analyze complex thermal processes
- Set  $\Delta T_{min}$  between hot and cold streams the minimum energy requirements (and therefore the maximum energy recovery) can be estimated
- Energy savings compared to the current scenario can be estimated as well as the new operating cost
- The optimal value of  $\Delta T_{min}$  is the result of an optimization: best trade-off between operating and investment cost





## Questions?

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